

## **AMENDMENTS TO THE CLAIMS:**

This listing of claims will replace all prior versions and listings of claims in the application:

1. (Previously presented) Process for the gas-phase (co-)polymerization of olefins in a fluidized bed reactor using a Ziegler-Natta type catalyst, said process comprising the addition into the reactor of an organoaluminium cocatalyst and of a monohalogenated hydrocarbon compound,
  - a. wherein the molar ratio of the monohalogenated hydrocarbon compound to the cocatalyst is comprised between 0.02 and 0.2,
  - b. wherein the monohalogenated hydrocarbon compound is added to the reactor in an amount comprised between 0.625 to 40 moles of monohalogenated hydrocarbon compound per mole of transition metal of catalyst introduced into the reactor, and
  - c. wherein the monohalogenated hydrocarbon compound is n-butyl chloride.
2. (Previously presented) Process according to claim 1 wherein the Ziegler-Natta type catalyst is a silica supported Ziegler-Natta catalyst.
3. (Previously presented) Process according to claim 1 or 2, wherein the molar ratio of the monohalogenated hydrocarbon compound to the cocatalyst is maintained constant throughout the polymerization.
4. (Previously presented) Process according to claim 1, wherein the sole or main olefin is either ethylene or propylene, and the optional comonomer is selected from but-1-ene, pent-1-ene, hex-1-ene, 4-methylpent-1-ene and oct-1-ene.

5. (Previously presented) Process according to claim 1, wherein the monohalogenated hydrocarbon compound is diluted in a diluent in an amount comprised between 0.001 and 2 mole of monohalogenated hydrocarbon compound per 1 of diluent.

6. (Previously presented) Process according to claim 1, wherein the monohalogenated hydrocarbon compound is not added in admixture with the catalyst.

7. (Previously presented) Process according to claim 1, wherein the catalyst is a non-prepolymerized catalyst.

8. (Previously presented) Process according to claim 7, wherein the catalyst is a titanium magnesium silica supported catalyst which is directly introduced into the reactor.

9. (Previously presented) Process according to claim 1, wherein the cocatalyst is comprised between 0.02 and 0.15.

10. (Cancelled).

11. (Currently amended) Process according to claim ~~[[10]]~~ 1, wherein the amount in b. is between 0.625 and 10.

12. (Previously presented) Process according to claim 11, wherein the amount in b. is between 0.625 and 5.

13. (Previously presented) Process according to claim 5, wherein the diluent is selected from the group consisting of butane, pentane and hexane.